

Design Testing and Simulation of Heat treatment pipe inside Process Reactionally Vessel.

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Abstract: Chemical Process is widely carried out by using heat. Naphtha is a volatile commercial product which is obtained by the distillation process in petroleum refinery of coal tar. Petroleum naphtha is a name for the petroleum distillate which contains aliphatic hydrocarbons and boiling point higher than the gasoline and lower than kerosene. In the crude oil distillation the overhead liquid distillate is called virgin or straight naphtha. The virgin naphtha has the initial boiling point of about 35 °C and final boiling point of about 200°C. A vertical storage column is typically used to store these liquids. To maximize the storage capacity, these columns are usually very tall typically over 27 meters. Heat is used to maintain viscosity of naphtha that is stored. As naphtha has a non-linear thermal property after distillation it is in the semi-fluid form. If the temperature drops the fluid changes from semi-liquid to semi-solid form and can cause considerable damage to the system and becomes difficult for further processing. However if we heat from below, at time surface cooling occurs and this makes natural convection stop, and the heat never reaches the top layers. Hence to avoid this heat pipes are inserted from top to ensure efficient distribution of heat. In this project we will study the effect of thermal stress due the presence of embedded heat pipes and try to simulate the distribution of heat in the system using ANSYS. Furthermore, we will take a problem statement from the company on any one pressure vessel job that is currently going on in the company and design the entire vessel. This would help us in realizing the challenges that need to be overcome when taking a real time project at hand.

Keywords: Naphtha, Process Reactionally Vessel, Heat Pipe, Performance, Design Testing and Simulation.

I. INTRODUCTION

Naphtha is a liquid state petroleum product that boils from about 30°C (86°F) to approximately boils at 200°C (392°F), although there are different types or grades of naphtha within this extensive boiling range that have different boiling ranges (Guthrie, 1968; Good fellow, 1973; Weisermel and Aarpe, 1979; Francis and Peters, 1980; Hoff man, 1983; Austin`s, 1984; Chenie R, 1992; Speight, 1999; Hori, 2000). The term petroleum solvent is often used synonymously with naphtha.

The so-called petroleum ether solvents are specific-boiling-range naphtha ligroin. The special value of naphtha is as a solvent lies in its stability and purity.

A process reactionally vessel is a container designed to hold gases or liquids at a pressure substantially different from the ambient pressure. The pressure differential is dangerous, and fatal accidents have occurred in the history of process reactionally vessel development and operation. Consequently, process reactionally vessel design, manufacture, and operation are regulated by engineering authorities backed by legislation. For these reasons, the definition of a process reactionally vessel varies from country to country, but involves parameters such as maximum safe operating pressure and temperature, and are engineered with a safety factor, minimum design temperature (for brittle fracture), corrosion allowance and involve nondestructive testing, such as ultrasonic`s testing, radiographies and pressure tests, usually involving water, also known as a hydro-test, but could be pneumatically tested involving air or another gas.

II. LITERATURE REVIEW

Senthilkumar [1] has studied the finite element analysis of pressure vessels for determining the stresses in local area`s such as penetration. They found that O-ring grooves and other areas are difficult to analyze by hand. After testings the three dimensional, symmetric and axisymmetric model finite element analysis becomes a extremely powerful tool. For symmetric models shell elements and axisymmetric models using solid elements can be used. Local stress risers, unrealistic displacement becomes extremely important in this kind of analysis.

M Ram Ranjan. [2] developed pipe cooling system using three dimensional finite element programs for thermal analysis. For the modeling of pipe they adopted the line element method also the internal flow theory was applied for calculating the temperature variation of cooling water. For the model of concrete eight node isoperimetric solid element was introduced and two node iso-parametric line elements was taken to this solid element to implement pipe cooling effect into the analysis. Results shows that the temperature variation of cooling water is efficiently obtained by influence of internal flow theory and line element.

Jin Keum kim [3] studied the different factors which can affect the performance of the heat pipe while selecting the material. The properties which were considered while selecting the material are corrosion resistance, stress corrosion cracking potential, thermal and mechanical properties and temperature limitations, finally they concluded that ferrite and stainless steel alloys containing 12% chromium can be most cost effective. **Michael A. Porter Dennis H. Martens Pedro Marcal. [4]** presented the practical approach in the analysis of typical pressure vessel components. 3-D brick element was taken as the element type for solution as it takes less time and effort. Also suggested that finer mesh will produce more accurate results than a coarser mesh. Another important consideration in meshing is the aspect ratio of the elements. (1:1:1) for brick elements which means that square or cubic elements are best.

William et al. [5] has studied the improved treatment of residual stresses which are produced by welding in pipes and pressure vessels fabricated from ferritic steels. The residual stresses in piping and pressure vessels depend on the pipe wall thickness and the welding heat input. The estimate for axial residual stresses at the inside surface can be related with a linearized bending residual stress that has been shown to accurately predict the effect of welding residual stress on crack connected to the internal surface. **Khandekar et al. [6]** studied that the closed loop pulsating heat pipes are complex heat transfer systems with a very strong thermo-hydrodynamic coupling governing the thermal performance. Semi-empirical correlation has been developed to fit the available data based on non-dimensional numbers of interest.

Tian et al. [7] has experimentally characterized the performance of a cellular metal sandwich heat sink consisting of a crossed tube core with embedded heat pipes under forced air convection. The experimental results shows that on pressure loss and heat transfer rate is obtained as function of Reynolds number for selected values of input heat fluxes, and compared with those obtained for sandwich structures with woven textile cores. Also the heat pipe sample can dissipate more heat than the stainless steel wire mesh sample.

Hadi Khoramishad.[8] has given two approaches for carrying out a design-by-analysis which covers both the stress categorization method and the direct route method for checking global plastic deformation and against progressive plastic deformation. The pipe is discretized by an axisymmetric ring element with quadrilateral cross section with 4 nodes as it gives better results.

III. PROBLEM DESCRIPTION

1] As temperature drops or down the fluid changes from semi-liquid to semi-solid form. This will Cause considerable damage to the system and becomes difficult for further processing. Uneven thermal Stresses developed in the heat pipe. This could cause a serious damage to the structure.

2] Naptha is the petroleum product which is used as fuel or use as their accordance. But due to temperature variation, there is chances of pipe chock up because of the viscosity. Below the 35 degree Celsius, Naphta get solidified state and due to this pipe will bursted or chock up.

3] To maintain Naptha in liquid state, that means to maintain it at 35 to 40 degree Celsius. In old method, it maintain by Natural convection so it is difficult to distribute the heat in proper way.

IV. CASE STUDY

4.1 THE THICK WALL CYLINDER

Thick-wall cylinders are used widely in industry as process reactionally vessels, pipes, gun tubes, etc. in many applications the cylinder wall thickness is constant and the cylinder is subjected to a uniform internal pressure p_1 , a uniform external pressure p_2 , an axial load p , and a temperature change ΔT . Often the temperature change ΔT is a function of the radial coordinate r only. Under such conditions, the deformations of the cylinder are symmetrical with respect to the axis of the cylinder. [1]

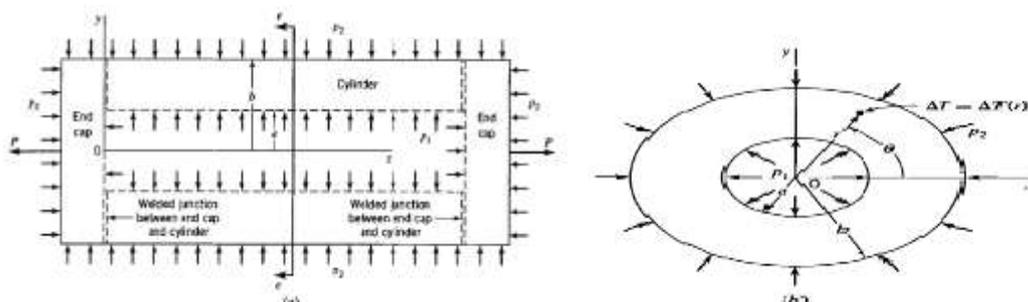


Fig 4.1 Closed cylinder with internal pressure, external pressure, and axial loads.

Furthermore, the deformations at a cross section sufficiently far removed from the junction of the cylinder and its end caps are practically independent of the axial coordinate z . In particular, if the cylinder is open and unconstrained, it undergoes ax symmetric deformations owing to pressure p_1 and p_2 and temperature changes $\Delta T = \Delta T(r)$, which are independent of z . If the cylinder's deformation is constrained by support or end caps, then in the vicinity of the supports or junction between the cylinder and end caps, the deformation and stresses will depend on the axial coordinate z .

4.2 STRESS COMPONENTS AND RADIAL DISPLACEMENT FOR CONSTANT TEMPERATURE

4.2.1 STRESS COMPONENTS

As there is no temperature change, $\Delta T=0$

The expressions for the stress components in a closed cylinder (cylinder with end caps) [2]

$$\sigma_{rr} = \frac{(p_1 a^2 - p_2 b^2)}{(b^2 - a^2)} - \frac{a^2 b^2}{r^2 (b^2 - a^2)} (p_1 - p_2) \quad \dots (1)$$

4.3 RADIAL DISPLACEMENT FOR A CLOSED CYLINDER

For no temperature change, $\Delta T=0$. Then the radial displacement u for a point in a thick-wall closed cylinder (cylinder with end caps).

The resulting expression for u is

$$u_{(\text{closed end})} = \frac{r}{E(b^2 - a^2)} \left[(1 - 2\nu)(p_1 a^2 - p_2 b^2) + \frac{(1 + \nu)a^2 b^2}{r^2} (p_1 - p_2) - \nu \frac{p}{\pi} \right] \quad \dots (2)$$

4.4 STRESSES AND DEFORMATIONS IN A HOLLOW CYLINDER

A Thick-wall closed-end cylinder is made of an aluminum alloy ($E=72\text{GPa}$ and $\nu=0.33$), has an inside diameter of 200mm, and has an outside diameter of 800mm. the cylinder is subjected to an internal pressure of 150 MPa. Determine the principle stresses, maximum shear stress at the inner radius($r=a=100\text{mm}$), and the increase in the inside diameter caused by the internal pressure.[2]

4.4.1 ANALYTICAL SOLUTION

The principal stresses are given by Equations (1) & (2).

$$\sigma_{rr} = \frac{(p_1 a^2 - p_2 b^2)}{(b^2 - a^2)} - \frac{a^2 b^2}{r^2 (b^2 - a^2)} (p_1 - p_2)$$

For the conditions that $p_2=0$ and $r=a$, these equations give

$$\sigma_{rr} = p_1 \frac{(a^2 - b^2)}{(b^2 - a^2)} = -p_1 = -150\text{MPa}$$

The maximum shear stress, given by

$$\tau_{\text{max}} = \frac{\sigma_{\text{max}} - \sigma_{\text{min}}}{2} = \frac{170 - (-150)}{2} = 160\text{MPa}$$

The increase in the inside diameter caused by the internal pressure is equal to twice the radial displacement given by

$$u_{(\text{closed end})} = \frac{r}{E(b^2 - a^2)} \left[(1 - 2\nu)(p_1 a^2 - p_2 b^2) + \frac{(1 + \nu)a^2 b^2}{r^2} (p_1 - p_2) - \nu \frac{p}{\pi} \right]$$

For the conditions $p_2 = p = 0$ and $r = a$. Thus,

$$u_{(r=a)} = \frac{p_1 a}{E(b^2 - a^2)} [(1 - 2\nu)a^2 + (1 + \nu)b^2]$$

$$= 0.3003\text{mm}$$

The increase in the inside diameter caused by the internal pressure is 0.6006mm.

4.5 NUMERICAL SOLUTION MODEL

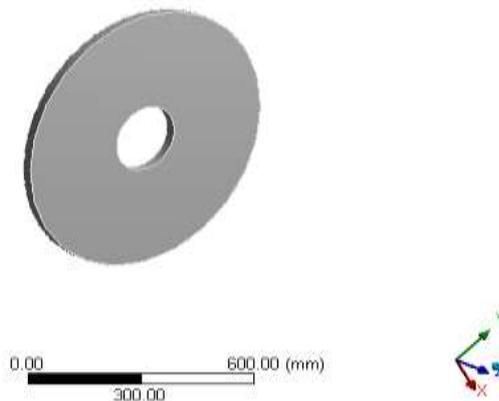


Figure 4.2 Model

Model was created having inside diameter of 200mm, and outside diameter of 800mm it is extruded to 30 mm keeping symmetry in both the direction. Then defined material properties are assigned to this geometry.

4.5.1 MATERIAL AND ITS PROPERTIES

Material Selected: Aluminum alloy

4.5.2 MESHING

METHOD: Hex Dominant method
 ELEMENT MIDSIDE NODES: Kept
 FREE FACE MESH TYPE: Quad/Tri
 NUMBER OF NODES: 29195
 NUMBER OF ELEMENTS: 5696
 ELEMENT TYPE: SOLID 186

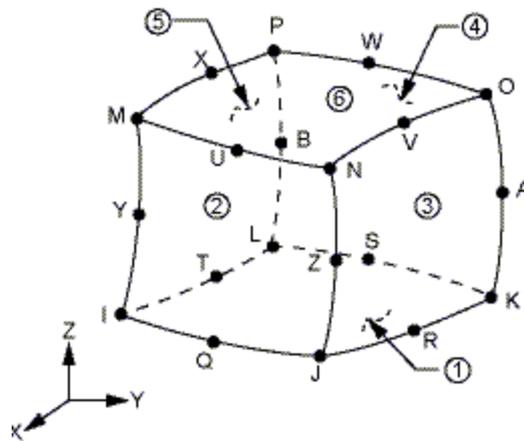


Fig 4.3 SOLID186 homogeneous Structural Solid Geometry

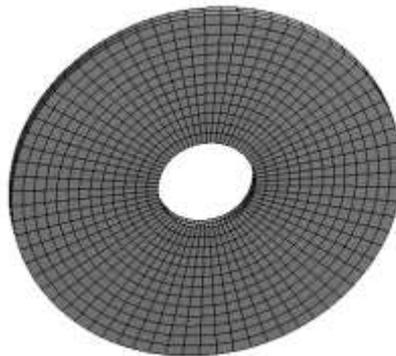


Fig 4.4 Meshing

Mapped meshing is done on both faces of the model to remove the irregularities in the meshing and making the mesh more refine.

4.6 BOUNDARY CONDITION

PRESSURE=150MPa

■ Pressure: 150. MPa

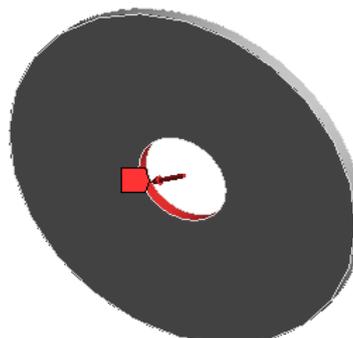


Fig 4.5 Boundary Condition

Figure 4.3 shows the model with boundary conditions. Pressure of the magnitude 150MPa is applied at the inner surface of the hollow cylinder. For cylinder no fix support is required since its structure itself acts as fix boundary conditions.

V. DESIGN OF PROCESS REACTIONALLY VESSEL

5.1 Design Data

Design a pressure vessel for the following specifications

Table 5.1: Design specification for process reactionally vessel

Sr No.	Parameter Description	Parameter Code	Value
1	Internal Pressure	P	0.05MPa
2	External Pressure	Po	Atm
3	Process Volume	Vp	205m ³
4	Expected Stagnant	VS	57m ³
5	Buffer Volume	Vb	50m ³
6	Vessel radius	R	2.5m
7	Tube porosity volume	TP	25
8	Radius of tube sheet	R	2.5m
9	Tube diameter	Td	200mm

5.2 INTERNAL DIMENSIONS CALCULATIONS

$$=20.5\text{m}^3 < V_s(57\text{m}^3)$$

Hence the vessel will be characterized as Process reactionary vessel.

5.3 CALCULATIONS FOR LOW PRESSURE APPLICATIONS (P < 1.4)

For P(0.05MPa) < 1.4MPa and Process reactionary vessel.

$$\text{NTD} = 11.6\text{m}$$

To determine L₁,

$$L_1 = 6.645\text{m}$$

5.4 RECALCULATION OF VOLUME CONSIDERING TUBESHEET THICKNESS

$$V_p = 1.1(V_p' + V_r) + 1.2(\pi \times T_d \times T_d)(T_p/400)N$$

Where,

$$V_p' = \text{process volume} = 205 \text{ m}^3$$

$$V_r = \text{residual volume} = 0.9754 \text{ m}^3$$

$$T_d = \text{tube diameter} = 0.2 \text{ m}$$

$$T_p = \text{tube porosity volume} = 25$$

$$N = \text{No of tubes} = 4$$

$$V_p = 1.1(205 + 0.9754) + 1.2(\pi \times 0.2 \times 0.2)(25/400)4$$

$$V_p = 226.61 \text{ m}^3$$

For Process reactionary vessel.

$$\text{NTD} = 12.823 \text{ m}$$

5.4.1 Internal pressure

$$\text{Assume } L_0 = (1.1) (\text{NTD})$$

$$L_0 = 1.1 \times 12.823$$

$$L_0 = 14.1053 \text{ m}$$

$$\text{Total Height } h_t = L_0 + 2 L_1$$

$$h_t = 27.3953 \text{ m}$$

$$P_i = 0.05 + \frac{\delta g h_t}{10^6}$$

$$= 0.3859 \text{ N/mm}^2 < 1.4 \text{ MPa}$$

5.5 MATERIAL PROPERTIES

SA 516 Grade70

Maximum allowable stress (S) = 20000 psi = 138 MPa

Modulus of elasticity E = 200 Gpa

Poisson's ratio $\mu = 0.29$

5.6 SHELL THICKNESS

$S = 138 \text{ MPa}$

$E_l = 0.7$ longitudinal seam efficiency (circ stress)

$E_e = 0.85$ circ seam efficiency (long. stress)

$P_i = 0.3859 \text{ MPa}$

$R = 2500 \text{ mm}$

From ASME SECTION VIII, div -I, UG27[3]

$$t_a = \frac{P_i \times R}{S \times E_l - 0.6 \times p_i}$$

$$t_a = 10.01$$

$$t_b = \frac{P \times R}{2SE_e + 0.4P}$$

$$t_b = 4.109$$

$$T_{\text{req}} = \text{Max}(t_a, t_b) + CA$$

$$T_{\text{req}} = 16.01 \text{ nt} = 18 \text{ mm}$$

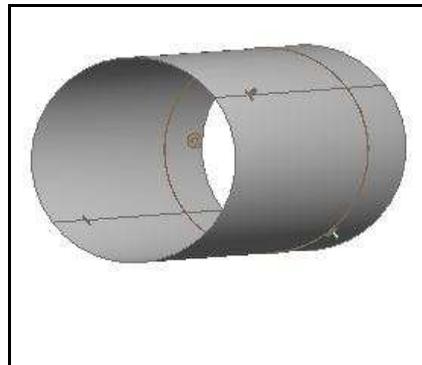


Fig 5.1 Shell render

5.6.1 Maximum Pressure

$$P_{i_1} = \frac{SE_l \times nt}{R_i + 0.6nt}$$

$$P_{i_1} = 0.6875$$

$$P_{i_2} = \frac{2SE_c \times nt}{R_i - 0.4nt}$$

$$P_{i_2} = 1.693 > 0.05 \text{ MPa}$$

$$P_{\text{max}} = 0.6875 > 0.3859$$

5.7 Thickness of head

Flat head

$$t_h = 200 \text{ mm}$$



Fig 5.2 flat head render

5.8 NOZZLE DESIGN

Nozzle design parameters,

Nozzle Material: SA-51670

$S_n = 138$ $E = 1$ (Nozzle efficiency)

$nt = 18 \text{ mm}$ Nozzle diameter = 100mm

Number of nozzle = 4

Drain Nozzle = 100mm

$$D_o = 100 + 2 \times 18 = 136$$

$$N_{wall} = 18\text{mm}$$

$$L_p = \text{Exterior projection of nozzle} = 3d_i \\ = 300\text{mm}$$

$$L_p = \text{Exterior projection of nozzle} = 0$$

$$nca = 6 \text{ (Nozzle corrosion allowance)}$$

$$P_n = 0.3859 \text{ MPa}$$

$$R_n = \frac{D_o}{2} - (N_{wall} - nca) \\ = 56 \text{ mm}$$

$$t_n = N_{wall} - nca$$

$$t_n = 12 \text{ mm}$$

$$t_i = N_{wall} - 2nca = 6 \text{ mm}$$

$$d = D_o - 2t_n = 112\text{mm}$$

$$(T_{req})_n = \frac{P_n \times R_n}{S \times E - 0.6 \times P_n} + nca \\ = 6.15 < 18\text{mm}$$

$$A_r = 1793.34 \text{ mm}^2$$

$$A_1 = 222.66 \text{ mm}^2$$

$$A_2 = 461.88 \text{ mm}^2$$

$$A_3 = -72\text{mm}^2$$

$$A_a = A_1 + A_2 + A_3$$

$$= 612.54 < A_r$$

Reinforcement pad required

5.8.1 REINFORCEMENT PAD DESIGN

$$L_0 = \text{NTD} + (\text{RF})\text{OD}$$

$$(\text{RF})\text{OD} = 1.1 \times 12.823 - 12.823$$

$$= 1.2823 \times 103\text{mm}$$

$$R = 641.15 \text{ mm}$$

$$T_{reqRP} = \frac{P_n \times R_n}{S_n \times E - 0.6 \times P_n} + nca \\ = 7.79\text{mm}$$

$$t_e = 9\text{mm}$$

$$A_1 = 222.6602 \text{ mm}^2$$

$$A_3 = -72\text{mm}^2$$

$$A_2 = 461.8819 \text{ mm}^2$$

$$A_5 = 10341 \text{ mm}^2$$

$$A_a = A_1 + A_2 + A_3 + A_5 = 10953.54 > A_r$$

For $D_p = 300\text{mm}$

$$A_a = 1530 > A_r$$

Optimum $D_p = 300\text{mm}$

$$= 6.42016 < 9\text{mm}$$

Hence design is safe

$$L_0 = (\text{NTD}) + (D_p)\text{RP}$$

$$L_0 = 13.213 \text{ m}$$

5.9 Calculation of pressure

$$h_t = L_0 + 2L_1$$

$$= 26.413 \text{ m}$$

$$P = 0.05 + \frac{\delta gh}{10^6}$$

$$P = 0.3759 \text{ MPa}$$

5.9.1 Shell thickness

$$t_a = \frac{P \times R}{S \times E - 0.6 \times P} + CA$$

$$= 7.19 + 6 = 13.191 < 15\text{mm}$$

5.9.2 For Nozzle

$$T_{reqN} = \frac{P_n \times R_n}{S_n \times E - 0.6 \times P_n} + nca$$

$$T_{reqRP} = \frac{P \times R_p}{S \times E - 0.6 \times P} + nca$$

$$= 6.1157 < 15mm$$

$$= 6.3018 < 9mm$$

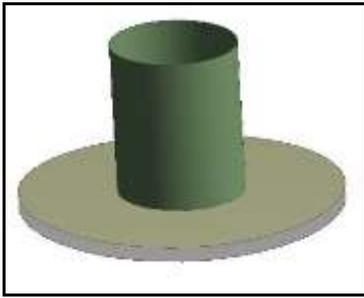


Fig 5.3 Nozzle with RF Pad render

5.10 SUPPORT SKIRT

Thickness of the skirt will be taken equal to the thickness of shell = 18mm

Total length of the skirt = 3m

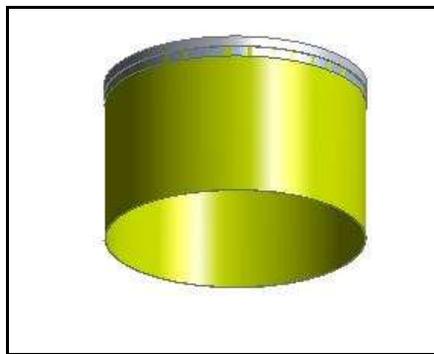


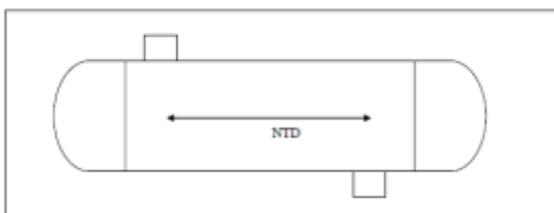
Fig 5.4 Support skirt render



Main stock Cylindrical length L0 = 11.9m

Buffer Stock Cylindrical Length L1 = 6.645m

Vessel Radius R= 2.5



Main Nozzle to Nozzle Centre Distance (Inlet/Outlet) NTD = 11.5m



Fig 5.5: Sectional view of vertical pressure vessel

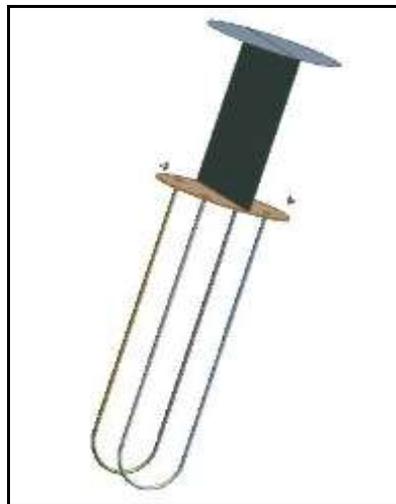


Fig 5.6 Embedded pipes with partition plate

VI. CONCLUSION

The structural and thermal analysis of embedded pipes inside pressure vessel is carried out using numerical simulation. Two models are simulated at different load conditions. After finalizing the model thermal analysis of u-shape embedded heat pipe were simulated. The temperature of naphtha heavy oil is between the ranges of 30-35 oC after 1900 seconds. So it can be concluded that these temperatures are within the acceptable limits.

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